

Review of NETL's Supercritical CO₂ (sCO₂) Techno-economic Analyses

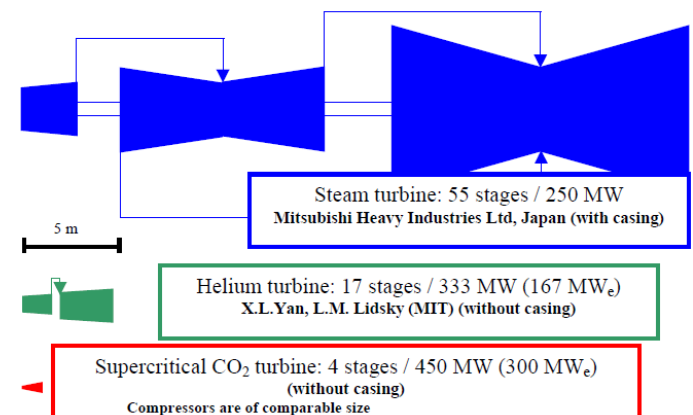
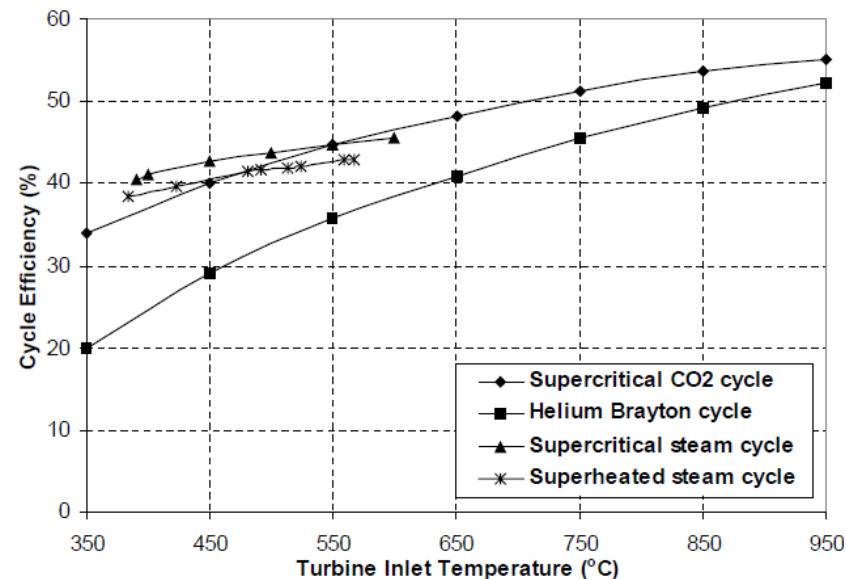
Nathan Weiland, Wally Shelton,
Travis Shultz, Charles White

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Why Supercritical CO₂ (sCO₂) Power Cycles?



- Applicable to multiple heat sources (nuclear, solar, fossil, waste heat) for indirect heating
- Potential for higher efficiency relative to traditional power cycles
 - High thermal recuperation rejects less heat to the environment
 - Single phase fluid heat transfer
 - Reduced cycle compression power near the CO₂ critical point
- Reduced turbomachinery sizes due to higher working fluid density
- CO₂ is generally stable, abundant, inexpensive, non-flammable, and less corrosive than H₂O

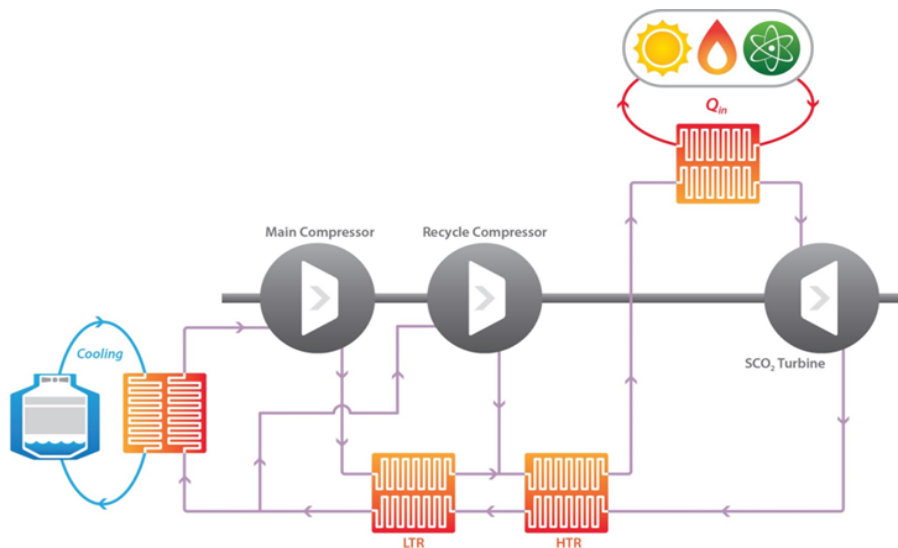


sCO₂ Cycles for Fossil Energy Applications



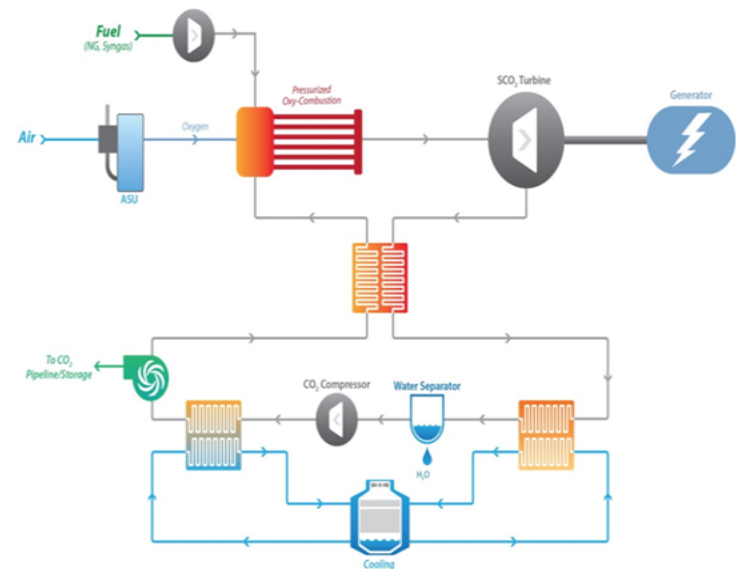
Indirectly-heated cycle

- Applicable to advanced combustion boilers
- Incumbent to beat: USC/AUSC boilers
- High fluid density, low pressure ratio yields compact turbomachinery
- Ideally suited to constant temp heat source
- Adaptable for dry cooling



Directly-heated cycle

- Applicable to IGCC and NGCC
- Incumbent to beat: Adv. F-, H-, or J- class Combined Cycle (NGCC or IGCC) w/ CCS
- Fuel flexible: coal syngas or NG
- 100% CO₂ capture at storage pressure
- Net water producer if air cooled



U.S. DOE Fossil Energy sCO₂ Power Cycle R&D Efforts



- **sCO₂ Power Cycles Base Program**

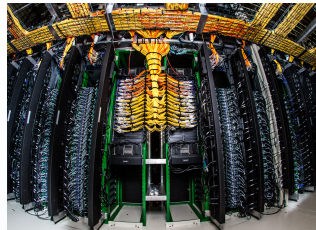
- Implemented through multiple Fossil Energy programs
- Combination of extramural projects and internal NETL research and analytical capabilities
 - Turbomachinery
 - Recuperators
 - Oxy-fuel Combustion
 - sCO₂ Heater Integration
 - Materials & Fundamentals
 - Systems Analysis

- **DOE sCO₂ Crosscut Initiative (STEP)**

- Collaboration between Fossil, Nuclear & Renewable DOE Offices
- Mission: Address technical issues, reduce risks, and mature technology to accelerate commercialization
- Objective/goal: Design, build, and test 10 MWe pilot sCO₂ facility (STEP)
 - Conceptual design studies complete
 - \$100 Million, 6 year build and test program to start in 2016

NETL Research and Innovation Center

Core Competencies



**Computational
Science &
Engineering**

**High-Performance
Computing**

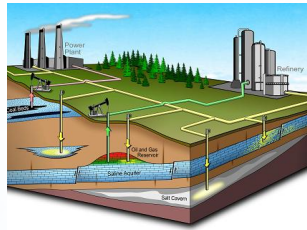
Data Analytics



**Materials
Engineering &
Manufacturing**

**Structural &
Functional**

**Design, Synthesis
& Performance**



**Geological &
Environmental
Systems**

**Air, Water &
Geology**

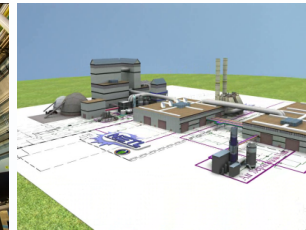
**Understanding &
Mitigation**



**Energy
Conversion
Engineering**

**Component &
Device**

**Design &
Validation**



**Systems
Engineering &
Analysis**

**Process &
System**

**Optimization,
Validation &
Economics**



**Program
Execution &
Integration**

Strategic Planning

**Project
Management**



U.S. DEPARTMENT OF
ENERGY

National Energy
Technology Laboratory

- **Techno-economic Evaluation of Utility-Scale Power Plants Based on the Indirect sCO₂ Brayton Cycle**
 - Final report under revision
- **Performance of an Integrated Gasification Direct-Fired Supercritical CO₂ Power Cycle**
 - Plant cost estimate nearing completion
- **Development of a dynamic sCO₂ plant model to assess control mechanisms and transient/part load performance of the 10 MWe STEP demo sCO₂ plant**
 - Preliminary analyses complete, model refinements ongoing

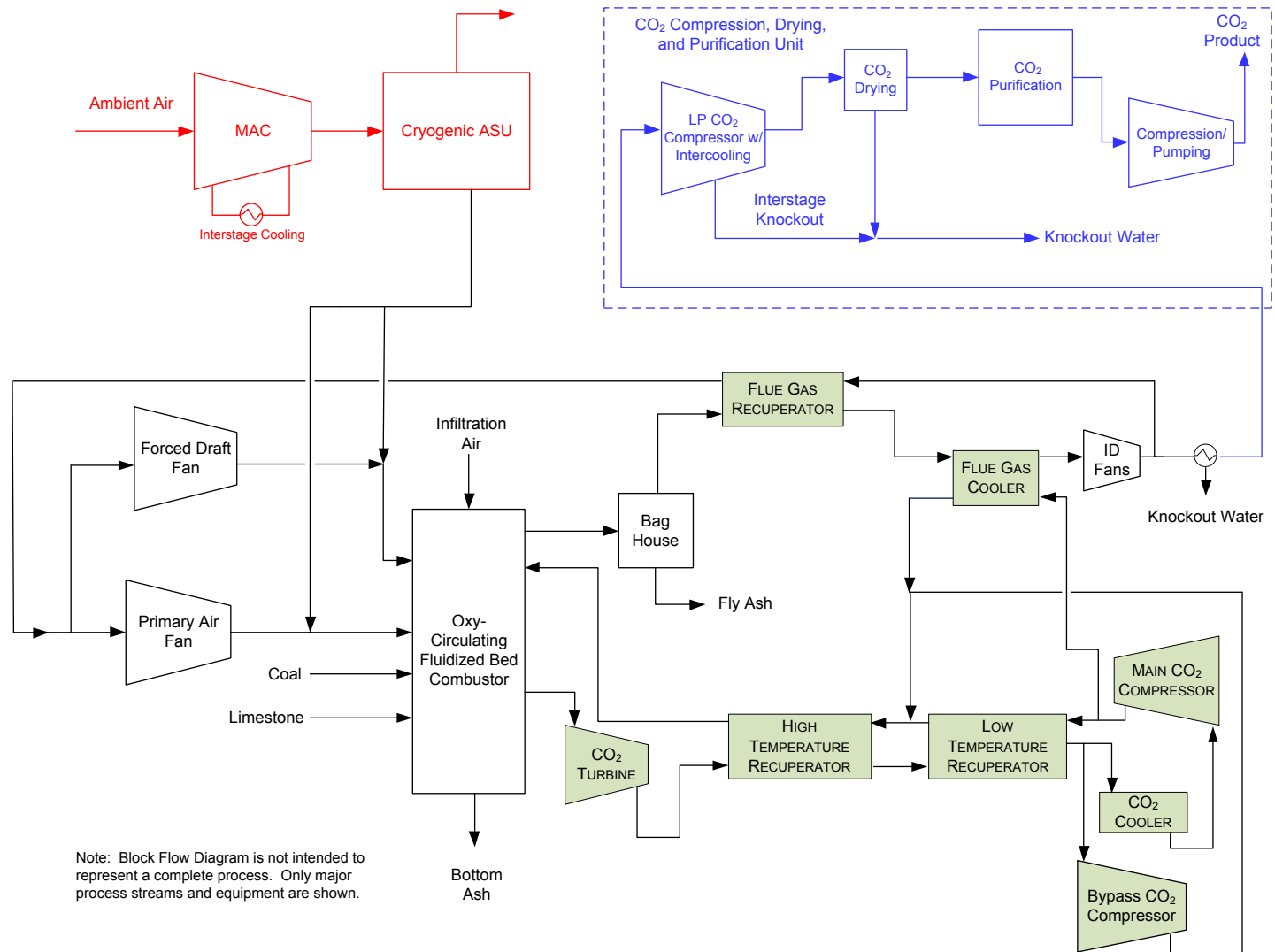
Utility-Scale Indirect sCO₂ Plants

Overview



- **Early work shows that the narrow temperature addition window of a recompression sCO₂ Brayton Cycle restricts boiler selection**
 - Modified Oxy-CFB boilers with CCS chosen for analysis
- **Reference: Oxy-Coal-Fired CFB Rankine Cycles with CCS (24.1 MPa/600 °C/620 °C)**
- **Oxy-Coal-Fired CFB sCO₂ Brayton Cycles with CCS: (620°C & 760°C)**
 - Recompression cycle with reheat and/or main compressor intercooling (4 combinations x 2 temperatures)
- **Performance Comparisons**
- **Economic Comparisons & Sensitivity of COE to TPC**
- **Potential for Improved Efficiency – Alternate Cycles**

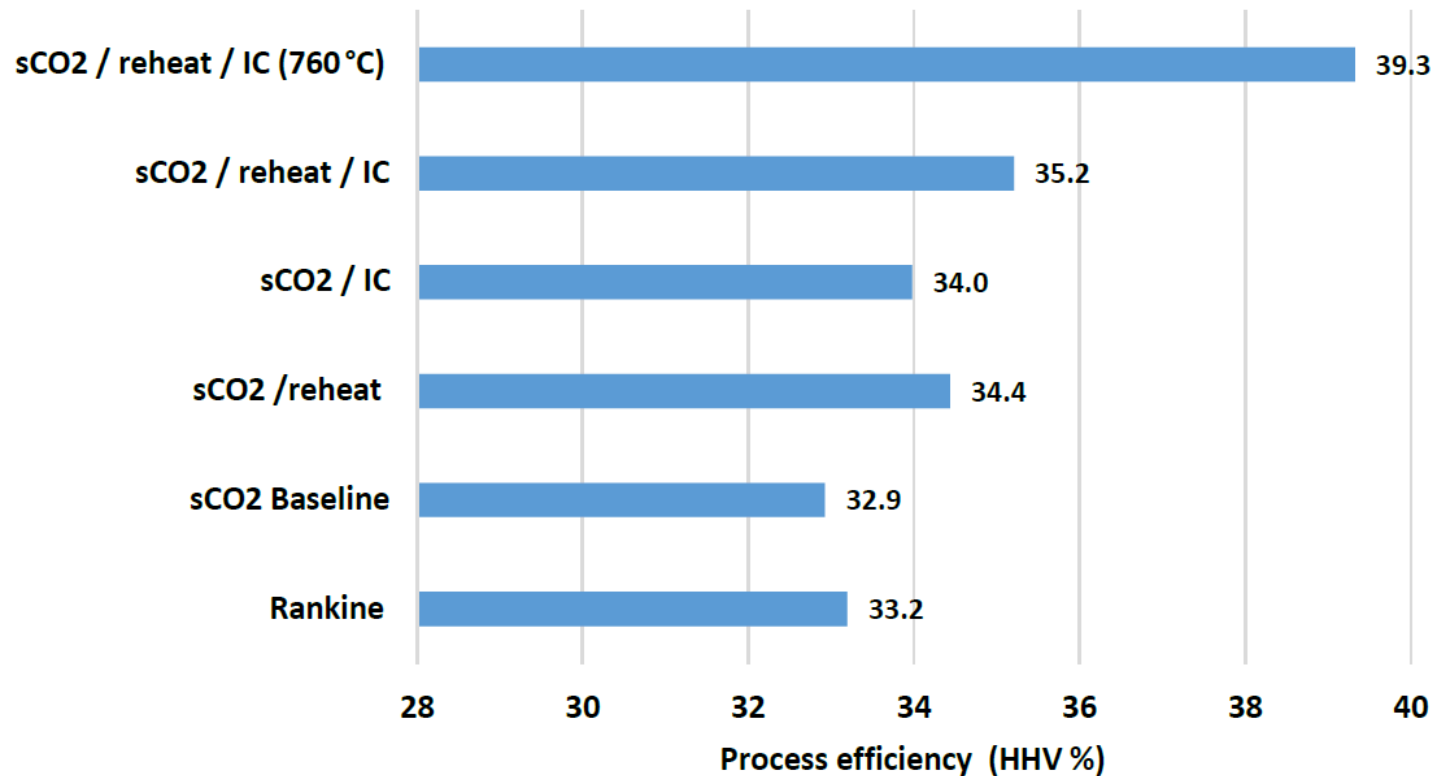
Oxy-Coal-Fired CFB Recompression sCO₂ Brayton Cycle



Indirect sCO₂ Plant Performance



Overall Plant Efficiencies (% HHV)



Indirect sCO₂ Summary and Conclusions

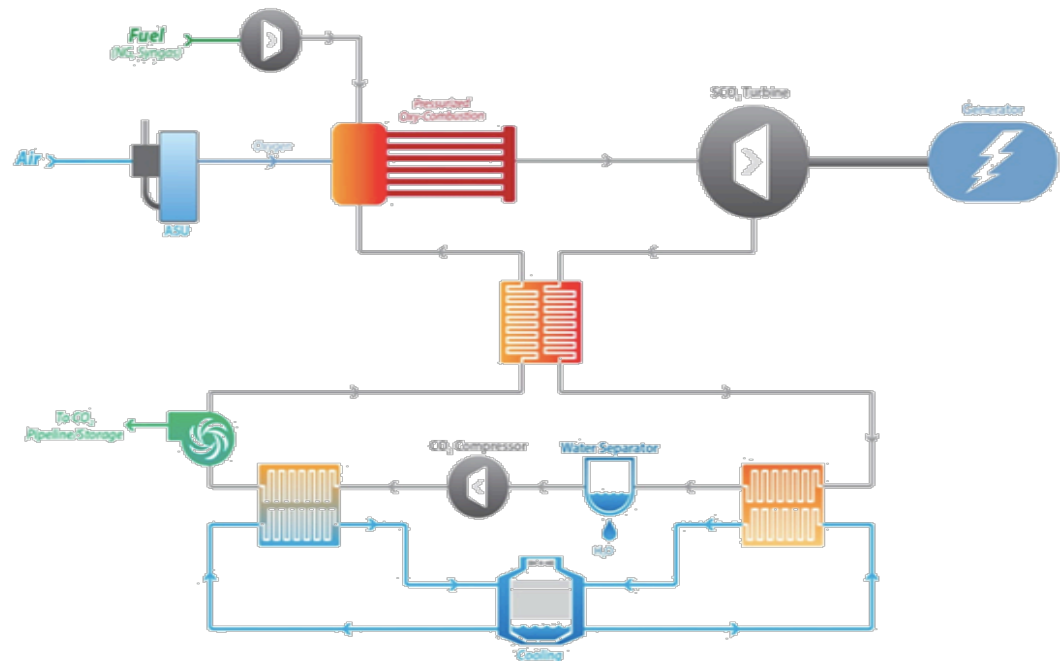


- **Objective - Compare sCO₂ Recompression Brayton Cycle(s) to a SOA Steam Rankine Cycle.**
- **Performance determined for four configurations, all showing performance improvement.**
- **At 620 °C turbine inlet temperature, the reheated and intercooled sCO₂ case shows a ~2 percentage points improvement in plant efficiency compared to the steam Rankine case.**
- **At the higher temperature (760 °C), the comparison to the Steam Rankine Cycle (620 °C) improves in overall efficiency to ~ 6 percentage points.**
- **Further optimizations of the configurations considered may be required to demonstrated an economic advantage.**
 - Condensing CO₂ cycles
 - Partial Cooling sCO₂ Cycle

Direct sCO₂ Cycle Analyses

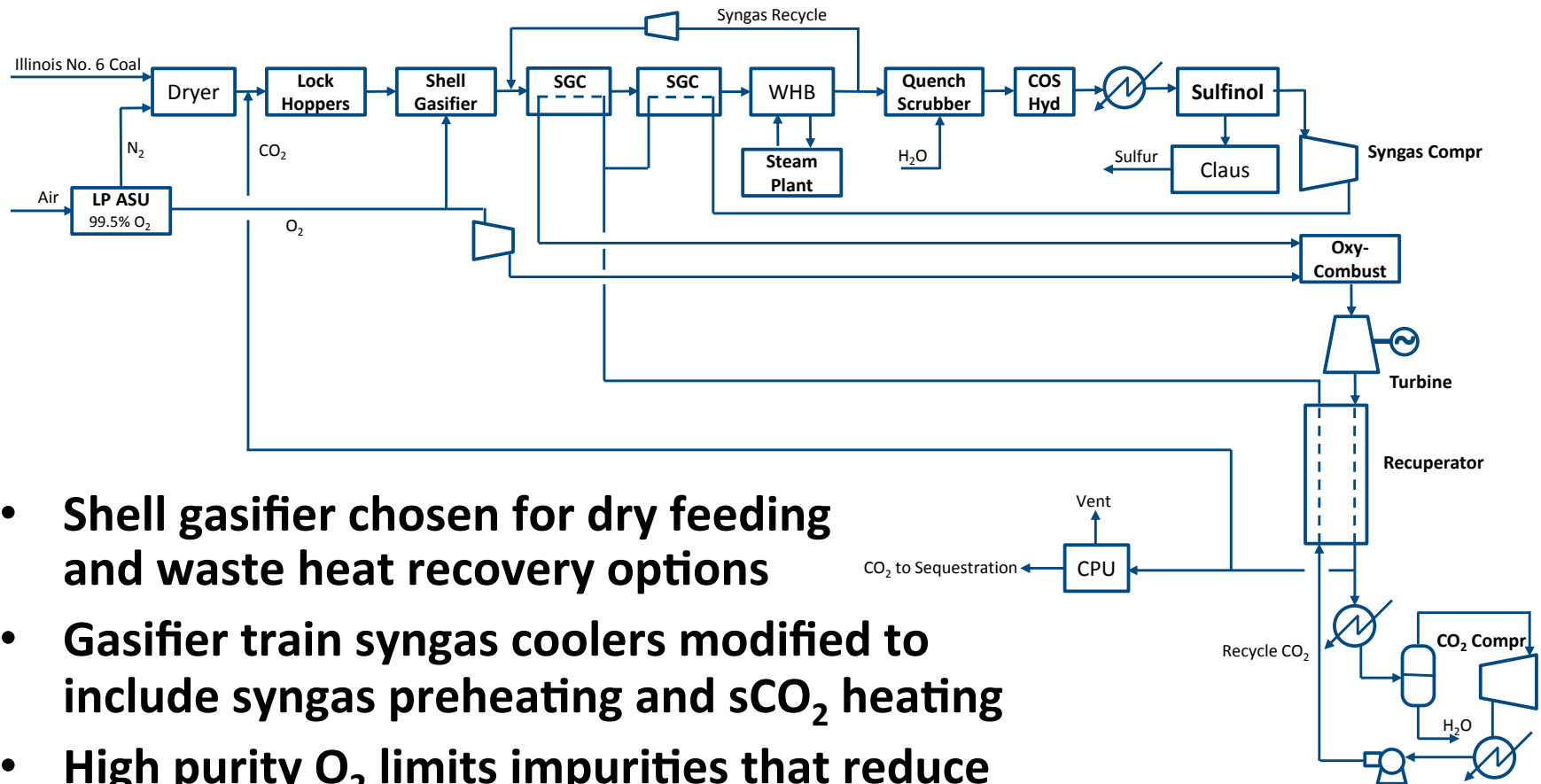


- Direct-fired sCO₂ power cycles are attractive due to their high efficiency and inherent ability to capture CO₂ at storage-ready pressures
- High pressures lead to high power density and reduced footprint & cost
- **Study Objectives:**
 - Develop a performance baseline for a syngas-fired direct sCO₂ cycle
 - Analyze sensitivity of performance and cost indicators to sCO₂ cycle parameters



Coal-fired Direct sCO₂ Plant

Block Flow Diagram



- Shell gasifier chosen for dry feeding and waste heat recovery options
- Gasifier train syngas coolers modified to include syngas preheating and sCO₂ heating
- High purity O₂ limits impurities that reduce direct sCO₂ cycle efficiency
- Syngas oxy-combustion within the sCO₂ cycle

Direct sCO₂ Conclusions and Future Work



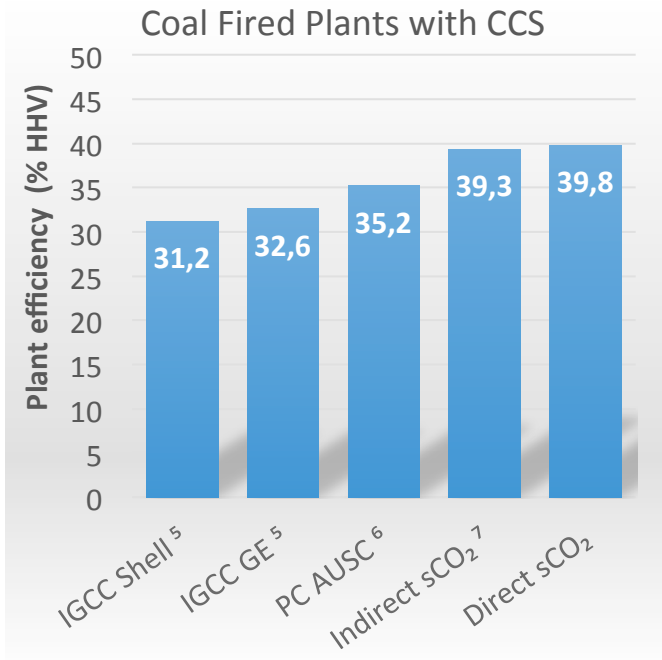
- **Conclusions:**

- Direct coal-fired sCO₂ cycle developed shows improved performance relative to IGCC and other reference cases
- Capital costs are expected to be lower than IGCC due to replacement of gas turbine and steam bottoming cycle
- Sensitivity studies provide guidelines for improving performance and reducing costs

- **Future Work**

- Incorporate the effects of turbine blade cooling flows (completed)
- Develop cost estimate for the improved baseline case (nearing completion)
- Extend analyses to development of natural gas-fired direct sCO₂ cycles

Parameter	IGCC	sCO ₂ Cycle	EPRI sCO ₂ Cycle ²
Net power output (MWe)	497	595	583
Net plant efficiency (HHV %)	31.2	39.8	39.6
Carbon capture fraction (%)	90	98	99
Captured CO ₂ purity (mol% CO ₂)	99.99	99.44	98.1



⁵ National Energy Technology Laboratory (NETL). (2010, November 2). Cost and Performance Baseline for Fossil Energy Plants Volume 1: Bituminous Coal and Natural Gas to Electricity. Pittsburgh, Pennsylvania.

⁶ Weiland, N., and Shelton, W. W. "Systems Analyses of Direct Power Extraction (DPE) and Advanced Ultra-Supercritical (AUSC) Power Plants," Crosscutting Research & Rare Earth Elements Portfolios Review, Pittsburgh, PA, April 18th, 2016.

⁷ Shelton, W. W., Weiland, N., White, C., Plunkett, J., and D. Gray. Oxy-coal-fired Circulating Fluid Bed Combustion with a Commercial Utility-size Supercritical CO₂ Power Cycle. The 5th International Symposium - Supercritical CO₂ Power Cycles, San Antonio, Texas, March 2016.

Other Current and Future sCO₂ Work within SEA



- **Pre-Screening of Indirect sCO₂ Cycle Integration Opportunities (complete)**
 - Evaluated the options for sCO₂ cycle integration with chemical looping combustion, magnetohydrodynamics, and fuel cell systems.
- **Process Systems Engineering Research Team**
 - Pressure-driven Aspen Plus Dynamics model of a 10 MW Indirect sCO₂ Recompression Brayton Cycle
 - Development of a multi-stage radial sCO₂ compressor in Aspen Custom Modeler
- **Development of a 1-D sCO₂ recuperator sizing/costing model**
 - Enables recuperator costing as a function of approach temperature, pressure drop, and materials of construction

It's All About a Clean, Affordable Energy Future



For more information on our sCO₂ efforts, contact:

Nathan.Weiland@netl.doe.gov, 412-386-4649 (NETL Research)

Rich.Dennis@netl.doe.gov, 304-285-4515 (DOE sCO₂ Program)

